

Pictorial Representation of Solid-Gas Equilibria at High Temperatures

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A pictorial representation of solid-gas equilibria is useful for studying the thermodynamics of a system under consideration. These diagrams show the stability regions of the species involved in a system as functions of pressures of two reacting gases. A computer program initially developed to plot the predominance area diagrams for metal-sulfur-oxygen (M-S-O) systems in roasting processes has been modified and generalized to handle any solid-gas system. This program has been utilized to plot the predominance area diagrams (PAD) for metal-sulfur-oxygen and metal-oxygen systems. The only data input required by the computer are the standard free energy values of all species existing in a system.

Using these diagrams, the optimum pressures of the reacting gases can be determined easily to form the desired species that are stable under these pressure conditions. The computer program may prove to be an important tool for studying thermodynamics of solid-gas systems in different processes like sulfidization roasting, chloridization roasting, volatilization roasting, direct reduction processes in sponge iron manufacturing, high-temperature oxidation, chemical vapor deposition, and reaction sintering of ceramics.

1 Introduction

THE predominance area diagram (PAD) for a system at a given temperature is a plot showing the predominance of the species existing in the system as a function of pressures of the reacting gases in the system. It is also known as a phase stability diagram. The predominance of various species is determined by thermodynamic considerations, namely by comparing the free energy changes associated with different chemical reactions under equilibrium condition.^[1] Because the thermodynamic data are available for many compounds^[2-4] at different temperatures, these diagrams can be plotted for many systems of interest and can be used in actual applications involving these systems.

To avoid the complications involved in the manual construction of these diagrams, a computer program was developed^[5] to plot such diagrams for M-S-O (metal-sulfur-oxygen) systems. The PADs for M-S-O systems are useful in studying the roasting processes involving metal sulfides^[6] and high-temperature corrosion of metals in sulfur atmosphere.^[7] Because the PADs for M-O (metal-oxygen) systems are also useful in many other processes,^[8] this program was modified to plot the PADs for any solid-gas system with at least two reacting gases, the logarithmic pressures of which are the coordinates of these diagrams.

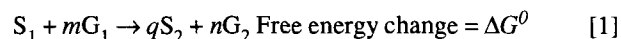
The manual construction of PADs involves many lengthy calculations and hence is a time-consuming and laborious process. To reduce the complexity of manual construction, it becomes necessary to limit the number of species to be considered and to use the practical knowledge of these systems to choose the species. To study the temperature dependence of relative stabilities of the species, PADs at various temperatures are required, which makes the task more difficult. This results in restricting the usage and application of these diagrams, which may be otherwise useful in many industrial processes. The computer program may prove to be useful in overcoming these hurdles and

may make it possible to plot PADs for more and more processes. This program can plot these diagrams at various temperatures for any system with no limit on the number of species involved. Thus, using this program, the thermodynamic stability of different species in any system over any range of pressures of the reacting gases and at any temperature can be studied. Using these diagrams, the optimum pressures of the reacting gases and temperature of operation for a process can be determined.

The PADs may be used to study the thermodynamics of sulfidization roasting, chloridization roasting, volatilization roasting, sponge iron production by direct reduction, high-temperature oxidation of metals, reaction sintering of ceramics, and chemical vapor deposition. This paper describes application of the computer program to obtain the PADs for Cu-S-O, Fe-S-O, Co-S-O, Mg-O, and Si-O and briefly discusses the results. A word of caution: The reliability of the PADs mainly depends on the reliability of the thermodynamic data, which vary from source to source.

2 Thermodynamics of Solid-Gas Reactions

A typical solid-gas reaction involving solids S_1 , S_2 and gases G_1 , G_2 can be expressed in an elementary manner as follows:



where m , n , and q are the numbers of molecules of G_1 , S_2 , and G_2 , respectively. Hence, the equilibrium constant for this reaction can be written as:

$$K = (pG_2)^n / (pG_1)^m \quad [2]$$

However, the free energy change is

$$\Delta G^0 = -2.303 RT \log K \quad [3]$$

where R is the gas constant, and T is the temperature in Kelvin. Thus, from Eq 2 and 3, one obtains:

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Table 1 Computer Output Listing the Input Data for the Cu-S-O System

| No. | Species | No. of Atoms of | | | Standard Free Energy | | | Symbol |
|----------------|-----------------------|---------------------|---------------------|---------------------|-----------------------------------|---------|---------|--------|
| | | Metal | Oxygen | Other | G ₀ =A+BTLogT+CT (cal) | | | |
| | | | | (A) | (B) | (C) | | |
| ----- | | | | | | | | |
| Reacting Gases | | | | | | | | |
| (1) | O ₂ | 0. | 2. | 0. | .000 | .000 | .000 | |
| (2) | SO ₂ | 0. | 2. | 1. | -125245.000 | .000 | 32.160 | |
| ----- | | | | | | | | |
| (1) | Cu | 1. | 0. | 0. | .000 | .000 | .000 | 1 |
| (2) | CuO | 1. | 1. | 0. | -37725.000 | -5.010 | 36.900 | 2 |
| (3) | Cu ₂ O | 2. | 1. | 0. | -40500.000 | -3.920 | 29.500 | 3 |
| (4) | CuS | 1. | 0. | 1. | -67000.000 | -3.110 | 42.720 | 4 |
| (5) | Cu ₂ S | 2. | 0. | 1. | -72775.000 | -6.220 | 43.590 | 5 |
| (6) | CuSO ₄ | 1. | 4. | 1. | -221625.000 | .000 | 103.250 | 6 |
| (7) | CuO.CuSO ₄ | 2. | 5. | 1. | -273205.000 | -13.340 | 177.420 | 7 |
| ----- | | | | | | | | |
| | Max-pG ₂ | Min-pG ₂ | Max-pG ₁ | Min-pG ₁ | (atm) | | | |
| | 0.1E+11 | 0.1E-09 | 0.1E+03 | 0.1E-22 | | | | |
| ----- | | | | | | | | |

$$-\Delta G^0/2.303 RT = n \log (pG_2) - m \log (pG_1) \quad [4]$$

A plot of this equation with $\log (pG_1)$ as x-axis and $\log (pG_2)$ as y-axis will give a straight line, because the left side of this equation is a constant quantity at a given temperature. When all such reactions of formation for the species involved in a system are obtained as a linear function of the logarithmic pressures of G_1 and G_2 , a PAD can be plotted by finding out the most stable species at given pressures of G_1 and G_2 .

One can see that if there are N species involved in a system, the number of such straight lines is equal to the number of equilibrium reactions, which is given by $[N(N - 1)/2]$. Hence, the construction of PADs for a system involving a large number of species, considering the calculations involved and the time required to do this manually, becomes too complicated. Consequently, the computer program described here simplifies the work and does not put any limit on the number of species to be considered.

3 Computer Program

The computer program, initially developed to plot the PADs for M-S-O systems,^[5] was able to plot these diagrams only for the reacting gases SO₂ and O₂. To study the roasting processes

for sulfides in the extraction of metals and the corrosion of metals in the presence of sulfur in chemical industries, the knowledge of PADs for various M-S-O becomes essential. Since such diagrams are useful to study any solid-gas reactions, the computer program was extensively modified to plot the PADs for all solid-gas systems (which may involve pure liquids). The new version of this program can be used to plot the PADs for any oxidation process, chloridization process, volatilization process, or even a reduction process (e.g., using H₂).

The logic of the program may be briefly described as follows. First, the chemical reactions between all the pairs of species S_i and S_j involving only the gases G_1 and G_2 other than the pair of species itself, are needed. The number of such reactions will be $[N(N - 1)/2]$, where N is the number of all the species in the system, which may possibly form under different pressure and temperature conditions. These are determined using the basic rules of chemistry. Once these are known, using the values of the standard free energy of formation for the species, the standard free energy change (as a function of temperature, e.g., $A + BT \log T + CT$, where A , B , and C are constants) associated with each of these reactions is calculated.

This is followed by calculations of the $\log K$ values for these reactions at a given temperature, which in turn provide the equations of the straight lines appearing in the PAD. Finally, to plot the PAD, the computer divides the diagram into several points,

Table 2 Computer Output Listing the Chemical Reactions Between All the Species in the Cu-S-O System

| No. | Chemical Reactions | Std. Free Energy Change Delta G=A+BTLogT+CT (cal) | | |
|------|---------------------------------------------------|------------------------------------------------------|---------|---------|
| | | (A) | (B) | (C) |
| (1) | 1.00 (Cu)+ .50 (O2)=(CuO) | -37725.000 | -5.010 | 36.900 |
| (2) | 2.00 (Cu)+ .50 (O2)=(Cu2O) | -40500.000 | -3.920 | 29.500 |
| (3) | 1.00 (Cu)+1.00 (SO2)=(CuS)+1.00 (O2) | 58245.000 | -3.110 | 10.560 |
| (4) | 2.00 (Cu)+1.00 (SO2)=(Cu2S)+1.00 (O2) | 52470.000 | -6.220 | 11.430 |
| (5) | 1.00 (Cu)+1.00 (SO2)+1.00 (O2)=(CuSO4) | -96380.000 | .000 | 71.090 |
| (6) | 2.00 (Cu)+1.00 (SO2)+1.50 (O2)=(CuO.CuSO4) | -147960.000 | -13.340 | 145.260 |
| (7) | 2.00 (CuO)=(Cu2O)+ .50 (O2) | 34950.000 | 6.100 | -44.300 |
| (8) | 1.00 (CuO)+1.00 (SO2)=(CuS)+1.50 (O2) | 95970.000 | 1.900 | -26.340 |
| (9) | 2.00 (CuO)+1.00 (SO2)=(Cu2S)+2.00 (O2) | 127920.000 | 3.800 | -62.370 |
| (10) | 1.00 (CuO)+1.00 (SO2)+ .50 (O2)=(CuSO4) | -58655.000 | 5.010 | 34.190 |
| (11) | 2.00 (CuO)+1.00 (SO2)+ .50 (O2)=(CuO.CuSO4) | -72510.000 | -3.320 | 71.460 |
| (12) | .50 (Cu2O)+1.00 (SO2)=(CuS)+1.25 (O2) | 78495.000 | -1.150 | -4.190 |
| (13) | 1.00 (Cu2O)+1.00 (SO2)=(Cu2S)+1.50 (O2) | 92970.000 | -2.300 | -18.070 |
| (14) | .50 (Cu2O)+1.00 (SO2)+ .75 (O2)=(CuSO4) | -76130.000 | 1.960 | 56.340 |
| (15) | 1.00 (Cu2O)+1.00 (SO2)+1.00 (O2)=(CuO.CuSO4) | -107460.000 | -9.420 | 115.760 |
| (16) | 2.00 (CuS)+1.00 (O2)=(Cu2S)+1.00 (SO2) | -64020.000 | .000 | -9.690 |
| (17) | 1.00 (CuS)+2.00 (O2)=(CuSO4) | -154625.000 | 3.110 | 60.530 |
| (18) | 2.00 (CuS)+3.50 (O2)=(CuO.CuSO4)+1.00 (SO2) | -264450.000 | -7.120 | 124.140 |
| (19) | .50 (Cu2S)+ .50 (SO2)+1.50 (O2)=(CuSO4) | -122615.000 | 3.110 | 65.375 |
| (20) | 1.00 (Cu2S)+2.50 (O2)=(CuO.CuSO4) | -200430.000 | -7.120 | 133.830 |
| (21) | 2.00 (CuSO4)=(CuO.CuSO4)+1.00 (SO2)+ .50 (O2) | 44800.000 | -13.340 | 3.080 |

uses the log *K* values to compare the stability of the species at each of these points, and finds out the most stable species using the criterion of the most negative free energy change of the reactions. This is carried out line by line for the whole diagram. To mark the predominance region of a species, the computer prints the character symbol of that species at the boundaries of that region. These symbols are fed to the computer as a part of the in-

put. These steps are repeated for various temperatures and for different systems.

3.1 Input

A typical input to this program is shown in Table 1. Significant values are the numbers of atoms of different elements and

Table 3 Computer Output Listing the Relations Between the Partial Pressures of SO₂ and O₂ for the Cu-S-O System

Temperature = 900. (Kelvin)

Relations between Log(pG₂) and Log(pG₁) for the above chemical reactions.

| | | | | | | |
|-------|---|-----------|---|----------------------------------|---|--------------------------------|
| (1) | (| 4.333)= | (| .000) Log (pG ₂) + | (| -.500) Log (pG ₁) |
| (2) | (| 5.921)= | (| .000) Log (pG ₂) + | (| -.500) Log (pG ₁) |
| (3) | (| -14.449)= | (| -1.000) Log (pG ₂) + | (| 1.000) Log (pG ₁) |
| (4) | (| -11.228)= | (| -1.000) Log (pG ₂) + | (| 1.000) Log (pG ₁) |
| (5) | (| 7.870)= | (| -1.000) Log (pG ₂) + | (| -1.000) Log (pG ₁) |
| (6) | (| 12.801)= | (| -1.000) Log (pG ₂) + | (| -1.500) Log (pG ₁) |
| (7) | (| -2.745)= | (| .000) Log (pG ₂) + | (| .500) Log (pG ₁) |
| (8) | (| -18.782)= | (| -1.000) Log (pG ₂) + | (| 1.500) Log (pG ₁) |
| (9) | (| -19.893)= | (| -1.000) Log (pG ₂) + | (| 2.000) Log (pG ₁) |
| (10) | (| 3.538)= | (| -1.000) Log (pG ₂) + | (| -.500) Log (pG ₁) |
| (11) | (| 4.135)= | (| -1.000) Log (pG ₂) + | (| -.500) Log (pG ₁) |
| (12) | (| -17.409)= | (| -1.000) Log (pG ₂) + | (| 1.250) Log (pG ₁) |
| (13) | (| -17.148)= | (| -1.000) Log (pG ₂) + | (| 1.500) Log (pG ₁) |
| (14) | (| 4.910)= | (| -1.000) Log (pG ₂) + | (| -.750) Log (pG ₁) |
| (15) | (| 6.880)= | (| -1.000) Log (pG ₂) + | (| -1.000) Log (pG ₁) |
| (16) | (| 17.670)= | (| 1.000) Log (pG ₂) + | (| -1.000) Log (pG ₁) |
| (17) | (| 22.319)= | (| .000) Log (pG ₂) + | (| -2.000) Log (pG ₁) |
| (18) | (| 41.699)= | (| 1.000) Log (pG ₂) + | (| -3.500) Log (pG ₁) |
| (19) | (| 13.484)= | (| -.500) Log (pG ₂) + | (| -1.500) Log (pG ₁) |
| (20) | (| 24.028)= | (| .000) Log (pG ₂) + | (| -2.500) Log (pG ₁) |
| (21) | (| -2.940)= | (| 1.000) Log (pG ₂) + | (| .500) Log (pG ₁) |

the standard free energies of formation as a function of temperature ($G^0 = A + BT \log T + CT$, cal.) for each of the species.

3.2 Output

The output consists of (1) a listing of all the data input (Table 1); (2) all the chemical reactions taking place in the system (Table 2); (3) all the relations between log G₁ and log G₂ for a given temperature, which are also the equations of the straight lines appearing on the PAD (Table 3); and (4) the PAD for the given temperature with the explanation of the symbols (Fig. 1).

4 Results and Discussion

The computer program has been used to plot the PADs for Cu-S-O, Fe-S-O, Co-S-O, Mg-O, and Si-O. These are shown in Fig. 1 through 7. To study the variation of relative stabilities of different species, the PADs at different temperatures for a system must be studied. The stability regions contract or expand without changing the slopes of the boundaries. This is because the variation in temperature does not change the chemical reaction, but it only affects the free energy change associated with the reaction. The slope of a boundary line is determined by the

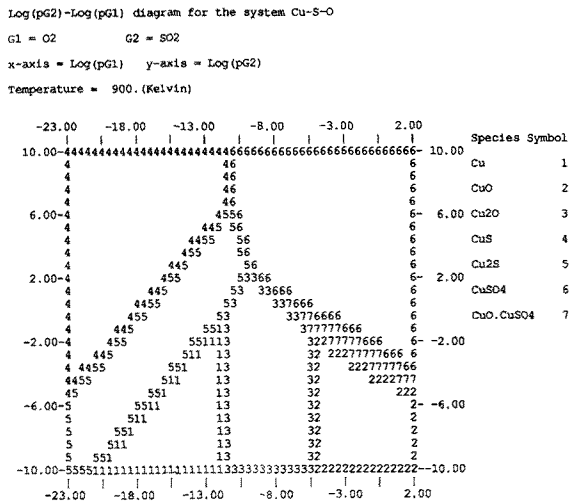


Fig. 1 Computer-plotted predominance area diagram for Cu-S-O system at 900 K.

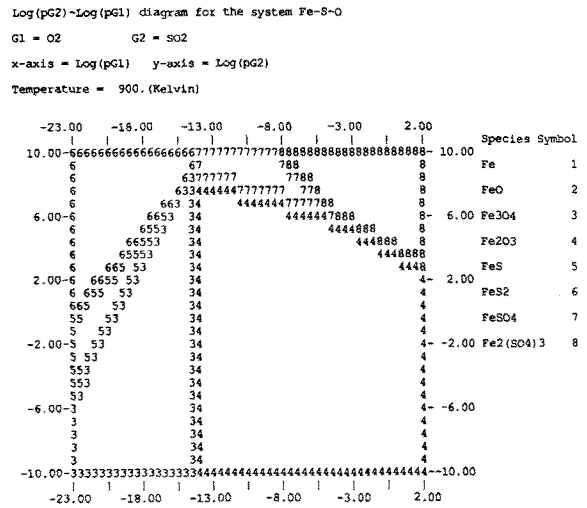


Fig. 2 Computer-plotted predominance area diagram for Fe-S-O system at 900 K.

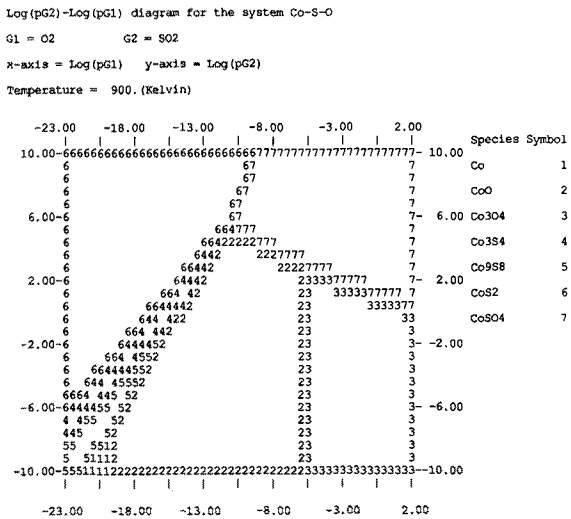


Fig. 3 Computer-plotted predominance area diagram for Co-S-O system at 900 K.

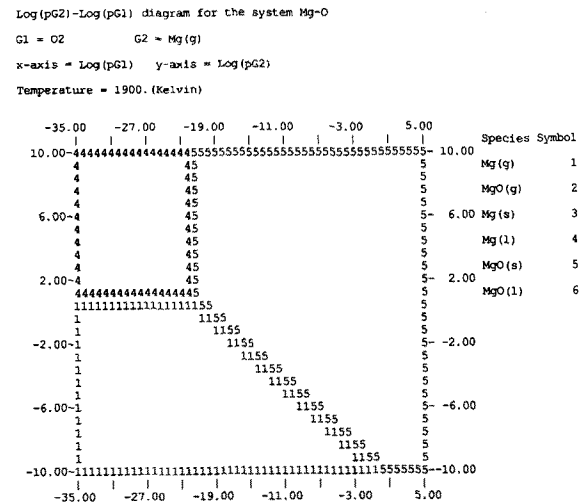


Fig. 4 Computer-plotted predominance area diagram for Mg-O system at 1900 K.

ratio of the numbers of the molecules of the gases reacting together to form one species from another, which remains unchanged.

4.1 M-S-O Systems

Figures 1, 2, and 3 show the PADs for Cu-S-O, Fe-S-O, and Co-S-O at 900 K. These PADs are useful when dealing with a single system, or with a mixture of two or more systems. The latter is often true in extractive metallurgy where the ore is always a mixture of two or more systems. For example, when copper ore is to be processed, the impurities containing iron sulfides and

possibly cobalt sulfides should be separated. If the ore is treated in such a manner that copper gets converted to copper sulfate, whereas iron and cobalt get converted to water-insoluble oxides, they can be separated easily by dissolving copper sulfate in water. The copper sulfate solution can be further processed by a hydrometallurgical route to produce fine copper powder in an autoclave by hydrogen reduction. The ore treatment required is necessarily an oxidation roasting process, in which the oxygen pressure and temperature is controlled so that the process yields the desired products. The optimum pressure and temperature values can be obtained by superimposing the PADs of Cu-S-O, Fe-S-O, and Co-S-O and then finding the pressure ranges of O₂

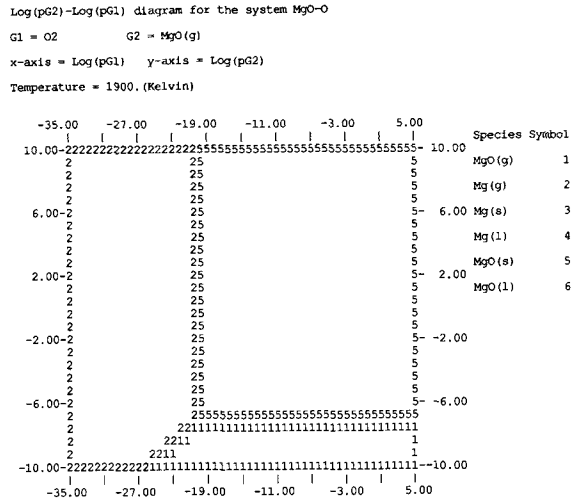


Fig. 5 Computer-plotted predominance area diagram for MgO-O system at 1900 K.

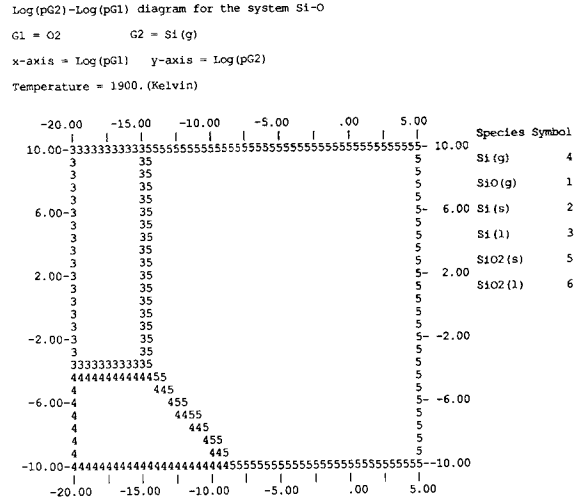


Fig. 6 Computer-plotted predominance area diagram for Si-O system at 1900 K.

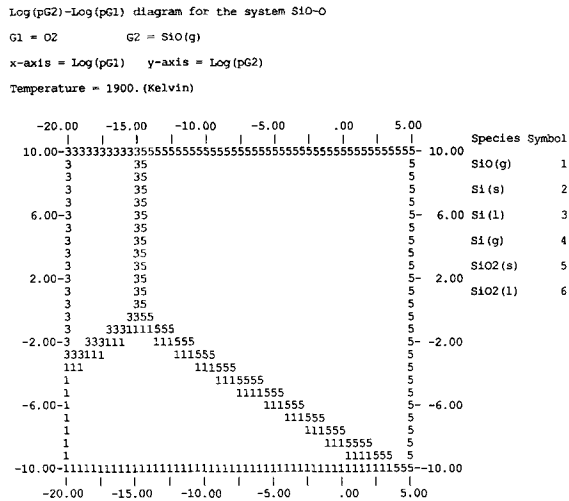


Fig. 7 Computer-plotted predominance area diagram for SiO-O system at 1900 K.

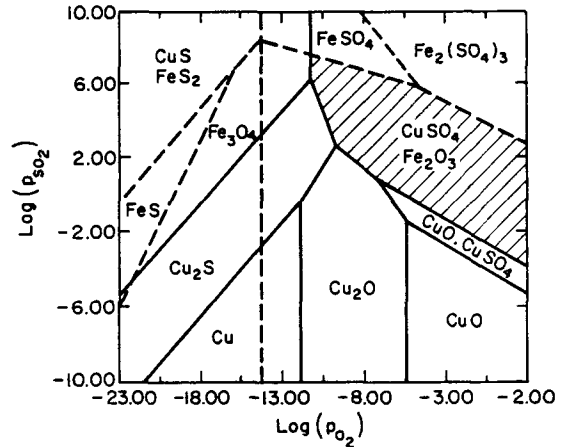


Fig. 8 Superimposed predominance area diagrams for Cu-S-O and Fe-S-O system at 900 K.

and SO₂ where copper sulfate, iron oxides, and cobalt oxides co-exist. This method can be repeated to separate iron and cobalt.

The procedure can be best illustrated by an example of the separation of copper and iron. Figure 8 shows the superimposed PADs of Cu-S-O and Fe-S-O at 900 K. If the pressures of O₂ and SO₂ are maintained at the values corresponding to the shaded region, the roasting process will yield CuSO₄ and Fe₂O₃. The products can be further treated with water to separate soluble CuSO₄ and insoluble Fe₂O₃.

In a highly corrosive atmosphere, the effect of sulfur on the corrosion of Fe can be studied using these diagrams. Such diagrams can also be plotted for other metal-sulfur-oxygen systems to study the corrosion resistance of those metals.

4.2 M-O Systems

In this system, two different PADs are possible, because the y-axis can represent either the partial pressure of metal or the partial pressure of metal oxide. Figure 4 shows the PAD with Mg and O₂ pressures as the coordinates and Fig. 5 shows the PAD with MgO and O₂ pressures as the coordinates, for the system Mg-O at 1900 K. Figure 6 shows the PAD with Si and O₂ pressures as the coordinates, and Fig. 7 shows the PAD with SiO and O₂ pressures as the coordinates, for the system Si-O at 1900 K.

These PADs are useful in sintering of MgO and SiO₂. One can study the formation of high-temperature phases at different vapor pressures of Mg or Si. These diagrams can be applied to reaction sintering of ceramics in synthesis of ceramics (*e.g.*, a PAD for Si-N can be used in the synthesis of Si₃N₄).

5 Conclusion

A computer program has been developed that can plot the predominance area diagrams for any solid-gas system at different temperatures of reactions. These diagrams are useful in studying the thermodynamics of solid-gas reactions at high temperatures, to obtain the optimum pressures of the reacting gases, and the optimum temperature of the process to obtain the desired reaction products. The PADs plotted using this program can be applied to many industrial processes like oxidation roasting, sulfidization roasting, chloridization roasting, volatilization processes, direct reduction processes (*e.g.*, sponge iron manufacturing), high-temperature corrosion of metals in different gaseous atmospheres, chemical vapor deposition processes, and reaction sintering of ceramics.

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